

Q1  
a)  $V_1 = 1 \text{ m}^3$

$$P_1 = 10 \text{ bar}$$

$$P_2 = 20 \text{ bar}$$

$$V_2 = ??$$

(i) ideal gas

$$\frac{P_1 V_1}{P_2 V_2} = \frac{m R T}{m R T}$$

$$V_2 = \frac{P_1 V_1}{P_2} = \frac{10 \times 1}{20} = \frac{1}{2} \text{ m}^3$$

(ii) water  $K = 2 \times 10^9 \text{ N/m}^2$

$$K = - \frac{P_2 - P_1}{\left(\frac{V_2 - V_1}{V_1}\right)} = - \frac{(20 - 10) \times 10^5}{\left(\frac{V_2 - 1}{1}\right)}$$

$$V_2 - 1 = \frac{-10 \times 10^5}{2 \times 10^9} = -5 \times 10^{-4}$$

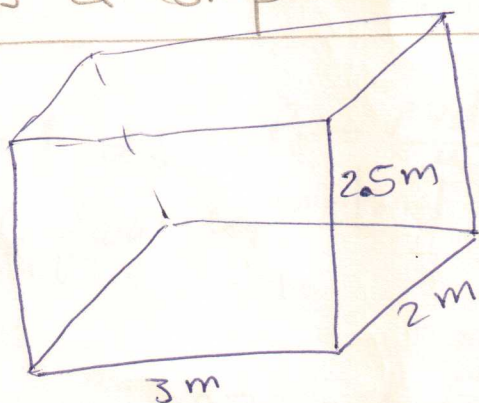
$$V_2 = 1 - 5 \times 10^{-4} = 0.9995 \text{ m}^3$$

from results

water is an incompressible fluid

ideal gas is a compressible fluid

(b)

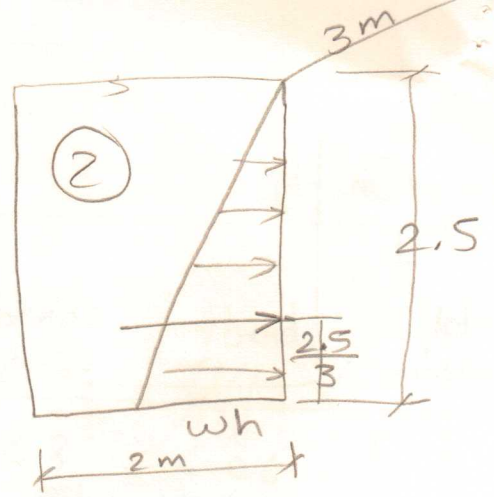
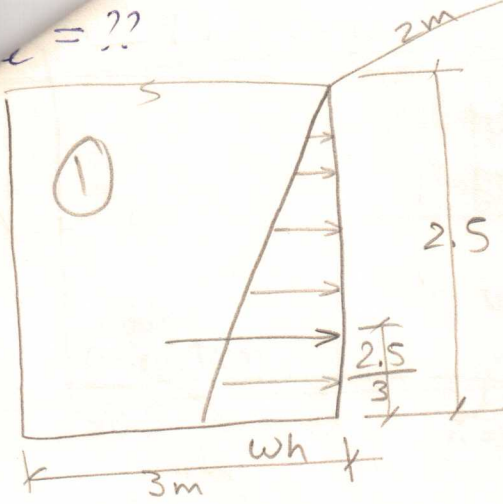


$$F_{\text{side}} = ??$$

$$F_{\text{bottom}} = ??$$

$$\rho_{\text{oil}} = \gamma_{\text{oil}} \rho_{\text{water}} = 0.9 \times 1000 = 900 \text{ kg/m}^3$$

$$W_{\text{oil}} = \rho_{\text{oil}} * g = 900 * 9.8 = 8820 \text{ N/m}^3$$



$$F_{\text{side}} = wh * \frac{h}{2} * B$$

$$F_{\text{side1}} = 8820 * 2.5 * \frac{2.5}{2} * 2 = 55,125 \text{ Newton}$$

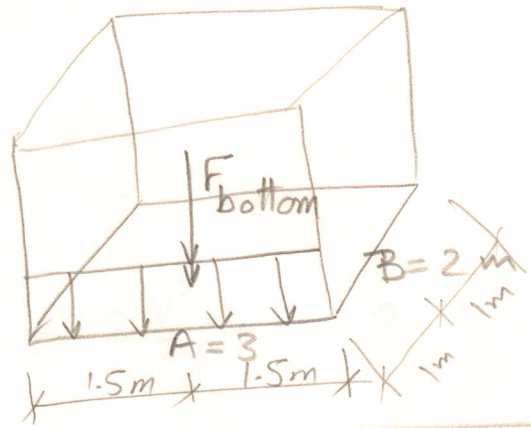
$$F_{\text{side2}} = 8820 * 2.5 * \frac{2.5}{2} * 3 = 82,687.5 \text{ Newton}$$

(ii)  $F_{\text{bottom}} = ??$

$$F_{\text{bottom}} = wh * A * B$$

$$= 8820 * 2.5 * 2 * 3$$

$$= 132,300 \text{ Newton}$$



Q2

a) i) x

higher total energy to lower total energy.

ii) x

friction loss and eddy loss

iii) ✓

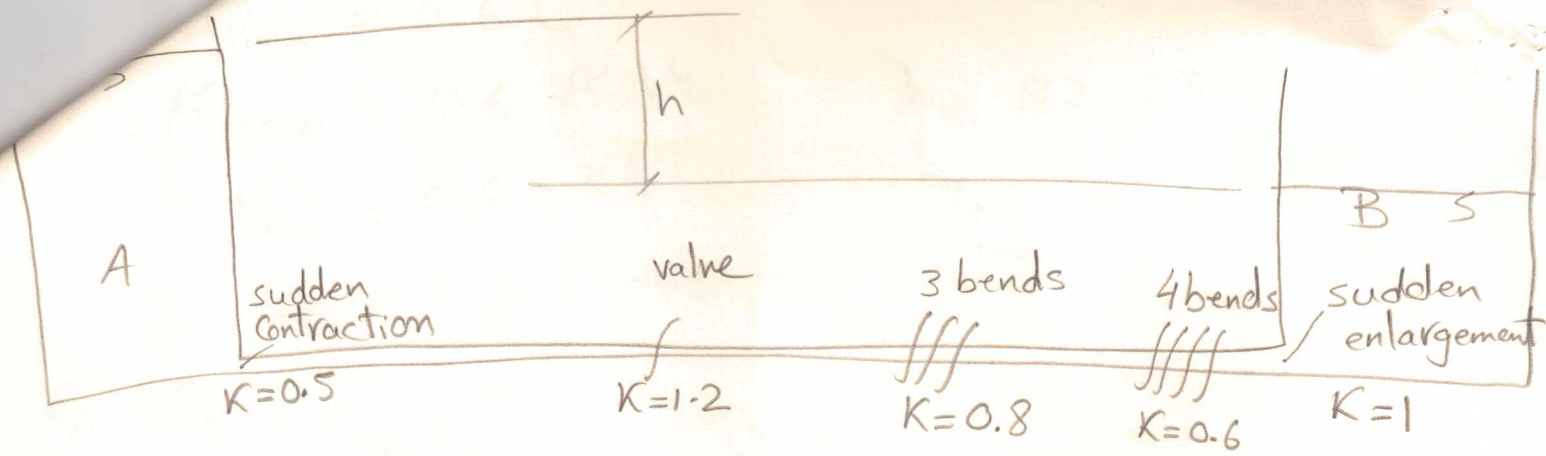
iv) x

$\mu \uparrow d \downarrow$   $Re = \frac{\rho v d}{\mu}$  expected to be small  
the flow expected to be laminar.

v) ✓

vi) x

$$C_{dv} = 0.97 \quad \& \quad C_{do} = 0.65$$



$$d = 15 \times 10^{-2} = 0.15 \text{ m}$$

$$l = 800 \text{ m}$$

$$f = 0.025 \quad \epsilon = 0.25 \times 10^{-3} \text{ m}$$

$$\textcircled{i} \quad h = ?? \quad Q = 60 \times 10^{-3} \text{ m}^3/\text{sec}$$

$$E_A = E_B + h_{\text{loss}}_{A \rightarrow B}$$

$$E_A - E_B = h_{\text{loss}}_{A \rightarrow B}$$

$$h = 0.5 \frac{V^2}{2g} + f \frac{l}{d} \frac{V^2}{2g} + 1.2 \frac{V^2}{2g} + 3 \times 0.8 \times \frac{V^2}{2g} +$$

$$4 \times 0.6 \times \frac{V^2}{2g} + 1 \times \frac{V^2}{2g}$$

$$h = \frac{V^2}{2g} \left( 0.5 + 0.025 \times \frac{800}{0.15} + 1.2 + 3 \times 0.8 + 4 \times 0.6 + 1 \right)$$

$$h = 7.185 V^2 \longrightarrow \textcircled{1}$$

$$Q = AV = \frac{\pi}{4} d^2 V$$

$$60 \times 10^{-3} = \frac{\pi}{4} (0.15)^2 \times V$$

$$\therefore V = 3.4 \text{ m/sec}$$

sub. in  $\textcircled{1}$

$$h = 82.83 \text{ m}$$

$$Q_{\text{new}} = 0.6 Q$$

$$A V_{\text{new}} = 0.6 A V$$

$$V_{\text{new}} = 0.6 * 3.4$$

$$V_{\text{new}} = 2.04 \text{ m/s}$$

$$h = 82.83 \text{ m}$$

$$h_{\text{loss value}} = ??$$

$$E_A - E_B = h_{\text{loss A} \rightarrow \text{B}}$$

$$82.83 = 0.5 \frac{V_{\text{new}}^2}{2g} + f \frac{l}{d} \frac{V_{\text{new}}^2}{2g} + h_{\text{loss value}} + 3 * 0.8 \frac{V_{\text{new}}^2}{2g} + 4 * 0.6 \frac{V_{\text{new}}^2}{2g} + 1 * \frac{V_{\text{new}}^2}{2g}$$

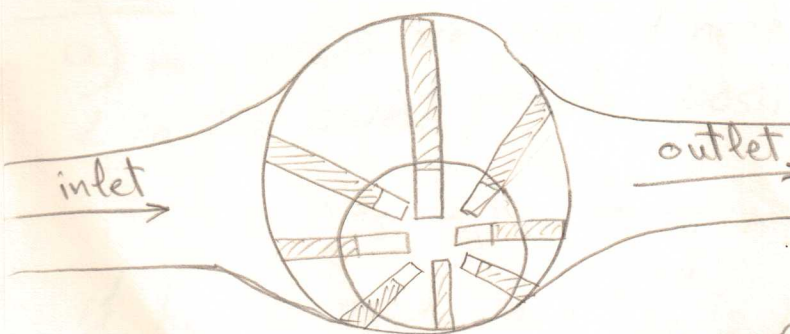
$$h_{\text{loss value}} = 82.83 - \frac{(2.04)^2}{2 * 9.8} \left[ 0.5 + 0.025 * \frac{800}{0.15} + 3 * 0.8 + 4 * 0.6 + 1 \right]$$

$$h_{\text{loss value}} = 53.18 \text{ m}$$

Q3

a) vane pump

\* positive displacement pump

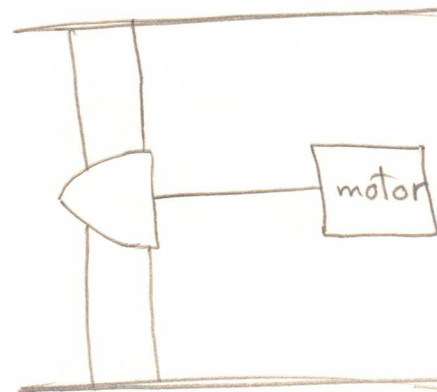
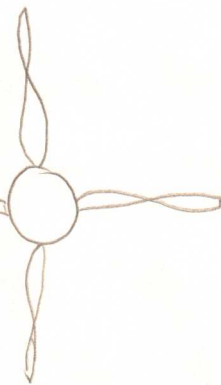


\* working at 500 bar pressure

\* expensive.

Axial flow pump

\* Dynamic head pump



\* gives very high discharge.  
low pressure head (upto 15m)

on pump three cylinders  $S = 60 \text{ cm} = 0.6 \text{ m}$

$$D = 30 \text{ cm} = 0.3 \text{ m} \quad h_{st} = 85 \text{ m} \quad Q = 80 \times 10^{-3} \text{ m}^3/\text{s}$$

$$h_{LS} = 1.2 \text{ m} \quad h_{LD} = 12 \text{ m} \quad v = 1 \text{ m/s}$$

$$\gamma_m = 0.9 \quad \gamma_{vol} = 0.98 \quad N = ?? \quad \text{Power} = ??$$

$$Q_{act} = \gamma_{vol} * \frac{\pi}{4} D^2 * S * \frac{N}{60} * \text{no. of cylinders}$$

$$80 \times 10^{-3} = 0.98 * \frac{\pi}{4} (0.3)^2 * 0.6 * \frac{N}{60} * 3$$

$$N = 38.5 \text{ rpm}$$

$$\begin{aligned} h_{pump} &= h_{st} + h_{loss_{total}} + \frac{v^2}{2g} \\ &= 85 + (1.2 + 12) + \frac{1^2}{2 * 9.8} \\ &= 98.25 \text{ m} \end{aligned}$$

$$\text{power} = \frac{\omega h_p Q}{\gamma_m} = \frac{9800 * 98.25 * 80 * 10^{-3}}{0.9}$$

$$= 35.2 \text{ watt}$$

Q4

a) All pumps are installed near suction tank ( $h_{es}$  min.)  
& in the lowest possible position w.r.t suction level ( $h_{ss}$  max.)

$$h_{ss} - h_{es} - \frac{v^2}{2g} > h_{vap} - h_{atm}$$

if  $h_{ss}$  is max. and  $h_{es}$  is min. then the L.H.S.  
will be greater than  $h_{vap} - h_{atm}$   
then we can avoid cavitation

Q	0	5	10	15	20	25
hm	70	74	73	65	53	40
eta	0	60	76	72	58	41
Sh.P.		60433	94132	132708	179103	239024

hst	hls	hld	KE	hss
50	5	10	0.2	-3

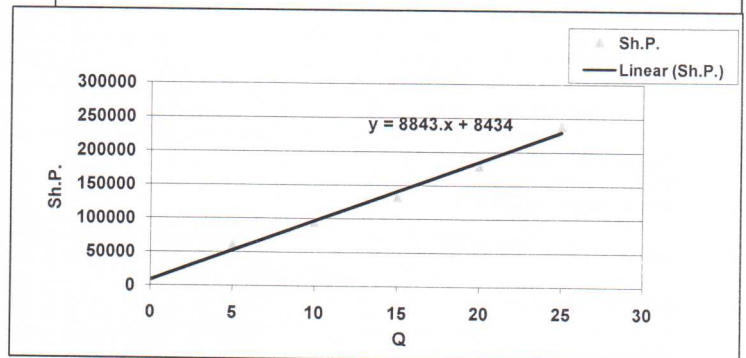
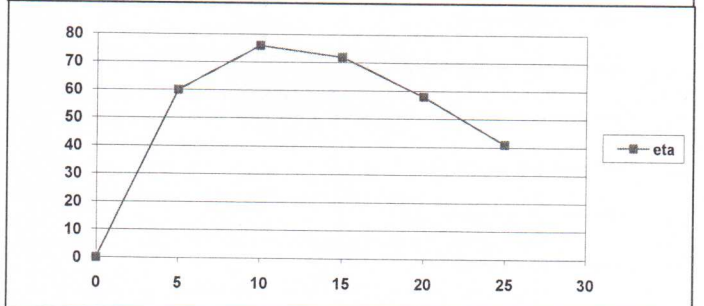
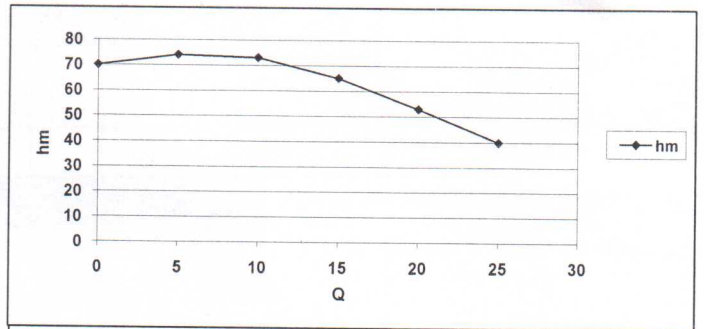
$$hp = hst + hlt + KE$$

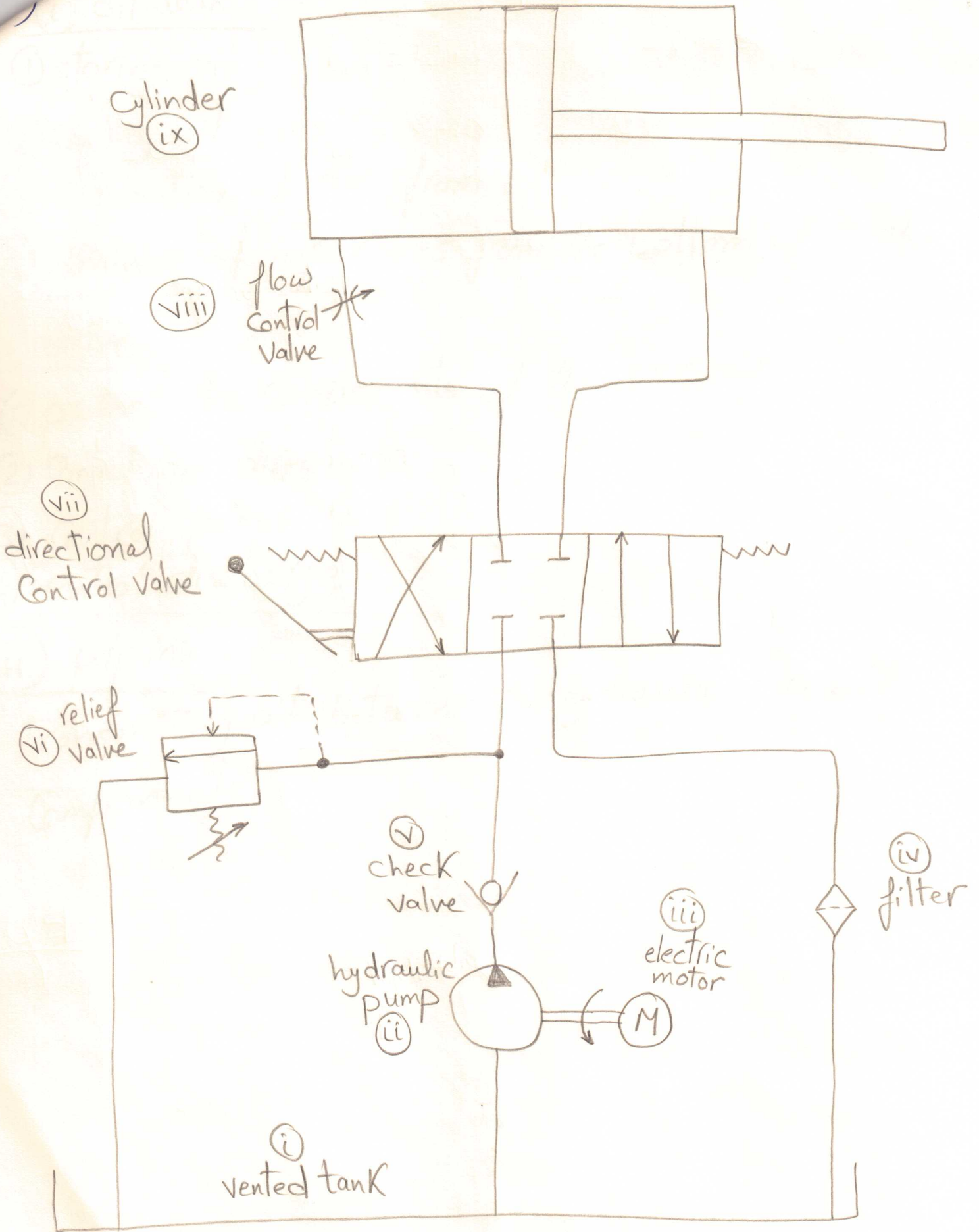
$$hp = 65.2 \quad m$$

$$hms = hss - hls - KE$$

$$hms = -8.2 \quad m$$

Sh.P. at operating point  
 Sh.P. = 132708 watt  
 Sh.P. = 132.71 kw





functions of :-

(i) oil tank

- ① storing oil
- ② Cooling oil
- ③ separation of air from oil
- ④ draining of impurities from the bottom of tank.

(ii) valves

- ① protect the components of the circuit
- ② Control oil direction
- ③ Control pressure
- ④ Control discharge

(iii) piping

transmitting oil between the hydraulic circuit components.